# 國立交通大學

# 機械工程學系

# 碩士論文

空氣噴流衝擊至一大直徑加熱圓盤之渦流結構與熱傳 特性研究



Vortex Flow and Thermal Characteristics Resulting from a Confined Round Jet of Air Impinging onto a

Large Heated Horizontal Disk

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# Vortex Flow and Thermal Characteristics Resulting from a Confined Round Jet of Air Impinging onto a Large Heated

#### **Horizontal Disk**

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#### 2008/6 于風城交大

# Vortex Flow and Thermal Characteristics Resulting from a Confined Round Jet of Air Impinging onto a Large Heated Horizontal Disk

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#### ABSTRACT

An experiment is carried out in the present study to investigate the vortex flow patterns resulting from a round air jet impinging over a large confined heated horizontal circular disk of 16 inch in diameter. In the present experiment the jet flow rate is varied from 0.4 to 10.0 (standard liter per minute) for the jet Reynolds number ranging from 27 to 676 with the injection pipe diameter  $D_j = 20.0$  mm and jet-disk separation distance H = 12.5mm and 25.0 mm. The temperature difference between the disk and the air injected at the inlet of the jet is varied from 0 to 14.0°C for the Rayleigh number Ra ranging from 0 to 7,340.

The results from the flow visualization for H=25.0 mm indicate that the vortex flow is characterized by the primary and/or secondary inertia-driven circular rolls along with several buoyancy-driven rolls. The number and strength of the buoyancy induced rolls increase with the buoyancy-to-inertia ratio, which can vary from 1 to 5. Besides, at a low  $Gr/Re_j^2$  slightly deformed circular buoyancy rolls prevail in the test section. For slightly higher  $Gr/Re_j^2$  the flow is dominated by the highly deformed curved rolls. The roll pattern becomes somewhat irregular for a further increase in

 $Gr/Re_j^2$ . For all cases examined here the vortex flow is unsteady at long time after the initial transients have died out and is irregular to a certain degree since the buoyancy effect is rather strong for the large impinging plate tested here. In addition to the roll deformation, the mutual pushing, merging and splitting of the buoyancy rolls occur nonperiodically in time. This unsteady and irregular vortex flow is also reflected in the data for the air temperature variations with time. Some quantitative buoyancy-driven vortex flow characteristics such as the size and location of the buoyancy rolls are summarized and correlated empirically. Moreover, a flow regime map is provided to delineate various induced vortex flow patterns and the boundaries separating various vortex flow patterns are also correlated empirically.

When the jet-disk separation distance is reduced to 12.5 mm for  $\Delta T$  varied from 8.0°C to 14.0°C (corresponding to the Rayleigh number ranging from 1,470 to 2,670), circular waves traveling in the radial direction and radial vortex rolls appear in the confined impinging jet flow. These waves are somewhat deformed and are not axisymmetric. The radial rolls originate in the stagnation region of the impinging jet and grow in size in the radial direction. The size of the radial rolls is also nonuniform in the circumferential direction. Besides, the moving waves and radial rolls can coexist in the flow. Moreover, the ranges of the jet Reynolds number and Rayleigh numbers leading to the new vortex flow patterns are determined. Flow regime maps delineating various vortex flow patterns including all inertia- and buoyancy-driven roll and wave patterns found here are given. And the boundaries among various vortex flow patterns are empirically correlated.

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# NONMENCLATURE

$\mathbf{D}_{j}$	Diameter of jet at the injection pipe exit (mm)
$D_{w}$	Diameter of disk (mm)
Gr	Grashof number, $g\beta\Delta TH^3/v^2$
g	Gravitational acceleration (m/s <sup>2</sup> )
Н	Jet-to-disk separation distance (mm)
$HD_j$	Ratio of the jet-disk separation distance to the jet diameter, $H\!/D_{j}$
$Q_j$	Jet flow rate (Standard Liter per Minute, slpm)
Z <sub>BR</sub>	The location of the buoyancy-driven roll near the center of jet
N <sub>BR</sub>	The number of the buoyancy-driven rolls
S <sub>BR2</sub>	The size of the second buoyancy-driven roll
S <sub>BR3</sub>	The size of the third buoyancy-driven roll
$S_{BR4}$	The size of the fourth buoyancy-driven roll
S <sub>BR5</sub>	The size of the fifth buoyancy-driven roll
$r, \theta, z$	Dimensional coordinates in cylindrical coordinate system
R, $\Theta, Z$	Dimensionless coordinates $r/R_c, \theta/360^\circ, z/H$
Ra	Rayleigh number, $g\beta\Delta TH^3/\alpha v$
Re <sub>j</sub>	Jet Reynolds number, $\overline{V_j}D_j/\nu$
T <sub>a</sub>	Ambient Temperature (°C)
$T_{f}$	Temperature of the heated disk ( $^{\circ}$ C)
$T_j$	Temperature of jet at the injection pipe exit (°C)
t	Time (sec)
$\overline{\mathbf{V}}_{j}$	Average velocity of the air jet at the injection pipe exit (m/s)

#### Greek symbols

α	Thermal diffusivity (	$(m^2/s)$
---	-----------------------	-----------

- $\beta$  Thermal expansion coefficient (1/K)
- $\Delta T$  Temperature difference between the heated disk and the air injected into the chamber (°C)
- v Kinematic viscosity  $(m^2/s)$
- $\Phi$  Non-dimensional temperature,  $(T T_j)/(T_f T_j)$
- $\rho$  Density (kg/m<sup>3</sup>)
- $\mu$  Dynamic viscosity (kg/ms)
- k Thermal conductivity  $(W/m^{\circ}C)$



#### Chapter 1

#### INTRODUCTION

#### **1.1 Motivation of the study**

It has been known for some time that the complex vortex flow and thermal characteristics driven by the buoyancy and inertia in a laminar gas jet impinging vertically downwards onto a heated horizontal disk confined a cylindrical chamber are relevant to the growth of crystal thin films from the metal-organic chemical vapor deposition (MOCVD) processes. In order to reduce the fabrication cost, we need to increase the wafer size and the gas flow over the large wafer will be affected by the buoyancy to a stronger degree. Thus the detailed understanding of the buoyancy driven flow and heat transfer in MOCVD processes is necessary in various microelectronic applications. It is also well known that the confined impinging jet flow depends on the jet Reynolds number, buoyancy-to-inertia ratio and nondimensional jet-disk separation distance. In the air jet impinging onto a large heated disk considered here the possible appearance of other vortex flow patterns, aside from the circular rolls, such as the radial rolls, bifurcation rolls, incomplete rolls, cells, etc needs to be investigated. This is still poorly understood. Specifically under what conditions these new vortex rolls appear needs to be explored. In the present study, we investigate the possible presence of new vortex flow structures and the associated flow and thermal characteristics in an impinging jet over a large confined heated circular plate. Effects of the jet Reynolds number, Rayleigh number and nondimensional jet-disk separation distance on the predicted flow and thermal structures will be examined in detail.

#### **1.2 literature review**

In a jet impingement flow over a large horizontal plate, we can identify three characteristic regions for an unconfined impinging jet and for a confined impinging jet, as schematically shown in Fig. 1.1[1] and Fig. 1.2[2], respectively. A potential core is formed which is called "the developing or free jet region" near the jet axis. Near the impinging plate, the jet impinges the plate and then is deflected away. We have the deflection zone of "the impingement flow region". Away from the stagnation point, the flow moves radially outwards and is called "the wall jet region". The literature relevant to the vortex flow and heat transfer in the jet impinging onto a heated plate is reviewed briefly in the following.

Considerable research has been carried out in the past to study the fluid flow and heat transfer in the round or slot jet impinging vertically downwards onto a large horizontal plate without confinement. Most of the studies focus on quantifying the highly efficient heat transfer associated with the high speed impinging jets. For example, heat or mass transfer in an unconfined air impinging jet was investigated by Hrycak[3] for  $D_p/D_j = 16$ , here  $D_p$  is the plate diameter and  $D_j$  is the nozzle diameter. Jambunathan et al.[4] and San and Shiao[5] studied an air jet impinging onto a rectangular plate for  $L/D_j = 5.5 \sim 166.7$  and  $W/D_j = 4.17 \sim 41.7$ , here L is the plate length and W is plate width. They found that there existed a maximum Nusselt number and they focused on effects of the jet size and flow in the stagnation region. Similar investigations on the cooling efficiency of air impinging jets were carried out by Chou and Hung [6] for L/W = 20 and by Chung and Luo [7] for  $L/W = 4\sim 10$ . Chou and Hung [6] proposed correlations for Nusselt number and found that if the velocity distribution is parabolic, there is a maximum Nusselt number in the stagnation region.

Moreover, Sahoo and Sharif [8] and Gao and Ewing [9] investigated a confined

impinging air jet respectively with L/W = 20 for a slot jet and  $L/D_j = 14.4 \sim 28.8$  for a round jet. The numerical modeling of slot air jet impingement cooling of a constant heat flux surface confined by a parallel wall conducted by Sahoo and sharif [8] found that when the jet Reynolds number increased, the centers of the primary and secondary inertia-driven rolls moved outward and when the buoyancy-inertia ratio increased, the strength and length of the secondary vortex decreases. While the investigation of the effects of the upper plate confinement on the heat transfer to round impinging jets exiting a long pipe examined by Gao and Ewing [9] found that the heat transfer resulting from the confined jet is smaller than that from the unconfined jet and when the jet Reynolds number increased , the location of the secondary maximum heat transfer on the impinging plate moved outward.

The flow field in a confined round jet impinging onto a rectangular target plate was investigated by Fitzgerald and Garimella [10] for  $L/D_j = 110$ ~55 and  $W/D_j =$ 15~55. Besides, a study of the flow field of a confined and submerged round impinging jet of FC-77 was conducted by Mortis and Garimella[11] for  $D_p/D_j = 15$ , here  $D_p$  is the diameter of the plate and  $D_j$  is the diameter of jet. Morris et al. [12] moved further to predict the flow-field in submerged and confined jet impingement by using the Reynolds stress model. They found that for an increase in the jet Reynolds number, the location of the center of the primary inertia-driven roll moved outward. Santen et al. [13, 14] studied mixed convection in radial flow between two horizontal plates in a confined air impinging jet with  $D_P/D_j = 25$ . They found that the value of the Rayleigh number affects the existence of non-axisymmetric flows and at high jet Reynolds number and low Rayleigh number, the non-axisymmetric flows can be suppressed and the three-dimensional flow changes to an axisymmetric flow. Chiriac and Ortega [15] carried out a numerical study of the unsteady flow and heat transfer in a transitional confined slot jet of air impinging onto a rectangular isothermal surface. They found that at the jet Reynolds number between 585 and 610, the flow becomes unsteady. Effects of the jet Reynolds number are investigated by Hsieh et al. [16-19] for a round impinging air jet confined in a vertical cylinder  $D_p/D_j=9.8\sim21.6$ . They reported that the jet Reynolds number can significantly influence the onset of the primary and secondary inertia-driven circular vortex rolls and if the jet Reynolds number is large enough, the tertiary inertia-driven roll can appear. Besides, the buoyancy-to-inertia ratio affects the onset of the buoyancy-driven roll and an increase of the ratio can induce a time-periodic flow and new roll but sometime can suppress the unsteady vortex flow. They also found that if the chamber top is tilted downward in the radial direction, the buoyancy-driven roll can be suppressed. Moreover, at a certain jet-disk separation distance the buoyancy-driven roll and inertia-driven roll are both large and can push and squeeze each other for certain ranges of Re<sub>j</sub> and Ra.

Santen et al.[20] examined a confined impinging jet of air with  $D_p/D_j = 25$  and noted that the onset of thermal instability was a function of Ra , Re<sub>j</sub> and Pr. A numerical study from Liu et al.[21] for a round confined impinging air jet observed that at high jet Reynolds number and Rayleigh number short radial rolls can be induced and many buoyancy driven rolls appear in the flow.

#### **1.3 objective of present study**

The above literature review clearly reveals that in a gas jet impinging onto a large heated disk the inertia and buoyancy driven vortex rolls aside from the circular rolls may be induced. But the patterns of these new vortex flows and the associated thermal characteristics remain largely unexplored. Experiment will be conducted in the present study to examine the possible presence of the inertia and buoyancy driven new vortex rolls in an air jet impinging onto a large heated disk with an upper parallel plate confinement. Attention will be focused on delineating the conditions leading to

the appearance of these rolls and the flow characteristics of these rolls.





Fig. 1.1 Flow structure associated with a circular unconfined jet impinging onto a flat plate.



Fig. 1.2 Flow structure associated with a circular confined jet impinging onto a flat plate.

#### **Chapter 2**

#### **Experimental Apparatus and Procedures**

In order to conduct the experiment at reasonably low cost, we use air as the working fluid to replace the inert gases normally employed in real CVD and RTP processes. In view of the similar thermodynamic and thermophysical properties for various gases, the results obtained here are still applicable to the CVD and RTP systems. The experimental system established in the present study to unravel the possible presence of new vortex flow structures and the associated thermal characteristics in a confined impinging air jet over a large horizontal heated disk and the test section are respectively shown in Figs. 2.1 and 2.2 schematically. The system consists of five major parts – the test section, temperature measurement unit, visualization unit, heating unit, and gas injection unit. The gas is first brought into the test section through an injector and then injected directly onto a circular heated disk. The major parts are briefly described in the following.

#### 2.1 Experimental apparatus

(1) **Test section:** The test section consists of an upper horizontal circular disk and a lower parallel circular heated disk. The upper circular disk is made of 9-mm thick circular glass plate to allow for the observation of the vortex pattern and is supported by several stainless steel bars to keep it at a required jet-disk separation distance. The stainless steel bars have skews so that we can adjust the vertical distance between the exits of the injection pipes and the heated disk. The structure of the lower circular heated disk will be described in the next subsection. Besides, the experimental system is very sensitive to disturbances from the surroundings. Therefore, the system is

confined in a small room formed by three wood planes and one black sheet of lint to reduce the effects of the disturbances from discharging the flow to the ambient surrounding.

(2) **Heating unit:** The heating unit is designed to maintain the lower circular disk at the preset uniform temperature during the experiment. It mainly includes a 15-mm thick high purity copper plate of 16-inch in diameter, acting as the impinging disk, which is directly placed on the heating elements. The edge of the heated disk is connected with a concentric insulated portion with an outer diameter of 25 inches. Besides, care is taken to insure that the upper surfaces of the heated disk and the insulated portion are kept at the same horizontal level so that the wall jet dose not experience a step change as it crosses the edge of the heated disk. After the jet impinges the heated disk, it moves in the radial direction over the heated plate and the insulated portion. Then the air is discharged into the ambient. More specifically, the heating unit consists of a resistance heating element, a holder and an insulator. The holder which is made of stainless steel can support the resistance heating element and the heated copper disk. The heater attached onto the back side of the copper plate is divided into 4 concentric zones (Fig. 2.3). Each zone is independently heated by a power supply with the D.C. current passing through the nickel coil placed on the stainless steel holder and its resistance is about 166 ohm. The entire heating unit is then placed on a Teflon plate. Additionally, to reduce the heat loss from the sidewall of the copper plate and Teflon plate, the lateral surface of the entire heating unit is wrapped with a 20.0-mm thick thermal insulation layer of superlon. A proper control of the voltage from each power supply allows us to maintain the copper plate at a nearly uniform temperature. Moreover, the copper plate temperature is measured by several corrected and calibrated T-type thermocouples at selected detection points located at 1-mm below the upper surface of the copper plate, which are fixed at the detection points through the small holes drilled from the backside of the plate (Fig. 2.4).

(3) Gas injection unit: The gas injection unit consists of a 2HP air compressor, a flow meter, a smoke generator, filters, pressure regulator, connection pipes and injector. In the experiment, air is drawn from the ambient by the compressor and sent into a 300-liter and 100-psi high-pressure air tank and is filtered to remove moisture and tiny particles. The installation of the high-pressure air tank intends to suppress the fluctuation of the air flow and extends the life of the compressor. Then, the air is mixed with smoke tracers in the smoke generator, regulated by the pressure regulator and later injected into the test section through a straight coaxial circular injection pipe. The downward vertical air jet issuing from the pipe outlet impinges directly onto the heated plate. In the present study, an injection pipe with a diameter of 20.0 mm is chosen and the straight portion of the pipe is 600-mm long. The length of the injection pipe is selected to ensure that they are long enough to allow us to have a fully developed air flow at the exit of the injection pipe. The distance between the exit of the injection pipe and the heated disk can be varied from 12.5 to 25.0 mm. The air temperature at 600-mm upstream of the exit of the injection pipe is measured by a corrected and calibrated T-type thermocouple. The measured value is considered as the temperature of the air injected into the test section since the whole injection pipe is thermally well insulated by a superlon insulation layer of 16-mm thick.

(4) **Visualization unit:** A smoke-tracer flow visualization technique is employed to observe the flow patterns resulting from the jet impinging onto the heated disk in the test section. The air flow pattern in the test section is illuminated by vertical and horizontal plane light sheets produced by passing parallel lights from an overhead projector through two adjustable knife edges. The experimental system is located in a darkroom to improve the contrast of the flow photos. The time variations of the flow

pattern during the entire transient stage from the top and side views are recorded by the Sony digital video camera DCR-PC330. The recorded images are later examined carefully in a personal computer.

(5) **Temperature measurement:** To understand thermal characteristics of the steady and unsteady vortex flows, the temperature of the air flow in the test section is measured by inserting a thermocouple probe laterally into the test section from the outside of the insulated portion. In the experiment, the thermocouple tip is positioned at selected vertical distances from the upper surface of the heated disk. More specifically, the thermocouple probe is an OMEGA (model HYPO) mini hypodermic extremely small T-type thermocouple implanted in a 1-inch long stainless steel hypodermic needle. The transient air temperature at selected locations in the test section is recorded by a recorder (YOKOGAWA MV200) after the vortex flow reaches a statistical state in which the initial transients in the flow have died out. The sampling rate of the recorder is 8 Hz for each data channel.

#### **2.3 Experimental procedures**

For each case the experiment starts with the air at the room temperature  $T_a$  compressed first into the high pressure tank and the smoke generator through the connection pipe, and then injected into the test section. The air moves first over the heated disk and finally leaves the test section. In the meantime the temperature of the heated disk and the air flow rate are controlled at the preset levels. As the air flow in the test section reaches steady or statistically stable state, we begin to visualize and record the vortex flow pattern in the space between the horizontal disks. Meanwhile, the air temperature is measured.

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Fig. 2.1 Schematic diagram of the experimental system.



Fig. 2.2 Schematic of the test section from side view showing the design of the heated disk.



Fig. 2.3 The heater consists of three parts: resistance heating element, holder and insulator.



Fig. 2.4 The locations of thermocouples.

#### **Chapter 3**

# DIMENSIONLESS GROUPS AND UNCERTAINTY ANALYSIS

The dimensionless groups relevant to the present problem and the analysis of the uncertainties of the variables in this experiment are briefly examined in this chapter.

#### **3.1 Dimensionless Groups**

The non-dimensional parameters associated with the flow considered here are the jet Reynolds number  $Re_j$ , based on the average velocity of the air jet  $\overline{V}_j$  at the injection pipe exit and the diameter of the injection pipe  $D_j$ , and the Rayleigh number Ra, based on the temperature difference between the heated disk and inlet gas  $\Delta T$  and the jet-disk separation distance H. They are respectively defined as

$$Re_{j} = \frac{V_{j}D_{j}}{v} = \frac{4}{\pi} \frac{Q_{j}}{vD_{j}},$$
(3.1)

and

$$Ra = \frac{g\beta(T_{f} - T_{j})H^{3}}{\alpha v} = \frac{g\beta\Delta TH^{3}}{\alpha v}$$
(3.2)

where  $\alpha$  is the thermal diffusivity, g is the gravitational acceleration,  $\beta$  is the thermal expansion coefficient, and v is the kinematic viscosity. Besides, we have the nondimensional jet-disk separation distance HD<sub>i</sub> defined as

$$HD_{j} = \frac{H}{D_{j}}$$
(3.3)

#### **3.2 Uncertainty Analysis**

An uncertainty analysis is carried out here to estimate the uncertainty levels in

the experiment. Kline and McClintock [22] proposed a formula for evaluating the uncertainty in the result F as a function of independent variables,  $X_1, X_2, \dots, X_n$ ,

$$\mathbf{F} = \mathbf{F} \left( \mathbf{X}_1, \mathbf{X}_2, \mathbf{X}_3, \dots, \mathbf{X}_n \right)$$
(3.4)

The absolute uncertainty of F is expressed as

$$\delta \mathbf{F} = \left\{ \left[ \left( \frac{\partial \mathbf{F}}{\partial \mathbf{X}_1} \right) \delta \mathbf{X}_1 \right]^2 + \left[ \left( \frac{\partial \mathbf{F}}{\partial \mathbf{X}_2} \right) \delta \mathbf{X}_2 \right]^2 + \left[ \left( \frac{\partial \mathbf{F}}{\partial \mathbf{X}_3} \right) \delta \mathbf{X}_3 \right]^2 + \dots + \left[ \left( \frac{\partial \mathbf{F}}{\partial \mathbf{X}_n} \right) \delta \mathbf{X}_n \right]^2 \right\}^{\frac{1}{2}}$$
(3.5)

and the relative uncertainty of F is

$$\frac{\delta F}{F} = \left\{ \left[ \left( \frac{\partial \ln F}{\partial \ln X_1} \right) \left( \frac{\delta X_1}{X_1} \right) \right]^2 + \left[ \left( \frac{\partial \ln F}{\partial \ln X_2} \right) \left( \frac{\delta X_2}{X_2} \right) \right]^2 + \dots + \left[ \left( \frac{\partial \ln F}{\partial \ln X_n} \right) \left( \frac{\delta X_n}{X_n} \right) \right]^2 \right\}^{\frac{1}{2}}$$
(3.6)  
If  $F = X_1^a X_2^b X_3^c$  ......, then the relative uncertainty is  

$$\frac{\delta F}{F} = \left[ \left( a \frac{\delta X_1}{X_1} \right)^2 + \left( b \frac{\delta X_2}{X_2} \right)^2 + \left( c \frac{\delta X_3}{X_3} \right)^2 + \dots \right]^{\frac{1}{2}}$$
(3.7)

where  $(\partial F/\partial X_i)$  and  $\delta X_i$  are, respectively, the sensitivity coefficient and uncertainty level associated with the variable  $X_i$ . The values of the uncertainty intervals  $\delta X_i$  are obtained by a root-mean-square combination of the precision uncertainty of the instruments and the unsteadiness uncertainty, as recommended by Moffat [23]. The choice of the variable  $X_i$  to be included in the calculation of the total uncertainty level of the result F depends on the purpose of the analysis. The uncertainties for the chosen parameters are calculated as follows:

(1) Uncertainty of the measured temperature difference,  $\Delta T = T_f - T_j$ 

$$\delta(T_{f} - T_{j}) = [(\delta T_{f})^{2} + (\delta T_{j})^{2}]^{\frac{1}{2}}$$
(3.8)

The dependence of the air properties k,  $\mu$ , and  $\rho$  on temperature (T in K) [24]

$$\mu = 1.448 \times 10^{-6} T^{1.5} / (T + 118)$$

$$k = 1.195 \times 10^{-6} T^{1.6} / (T + 118)$$

$$\nu = \mu / \rho$$
(3.9)

The uncertainties of the properties are

$$\frac{\delta k}{k} = \frac{T}{k} \frac{\partial k}{\partial T} \frac{\delta T}{T}$$

$$\frac{\delta \rho}{\rho} = \frac{T}{\rho} \frac{\partial \rho}{\partial T} \frac{\delta T}{T}$$

$$\frac{\delta \mu}{\mu} = \frac{T}{\mu} \frac{\partial \mu}{\partial T} \frac{\delta T}{T}$$
(3.10)

#### (3) Uncertainty of the Rayleigh number, Ra,

$$Ra = \frac{g\beta(T_{f} - T_{j})H^{3}}{\alpha \nu} = \frac{g\beta\Delta TH^{3}}{\alpha \nu}$$
(3.11)  
$$\frac{\delta Ra}{Ra} = \left[ \left(\frac{\delta g\beta}{g\beta}\right)^{2} + \left(3\frac{\delta H}{H}\right)^{2} + \left(\frac{\delta\Delta T}{\Delta T}\right)^{2} + \left(\frac{\delta\alpha}{\alpha}\right)^{2} + \left(\frac{\delta\nu}{\nu}\right)^{2} \right]^{1/2}$$
(3.12)

(4) Uncertainty of the jet Reynolds number, Rej,

$$\operatorname{Re}_{j} = \frac{V_{j}D_{j}}{v} = \frac{4}{\pi} \frac{Q_{j}}{vD_{j}}$$
(3.13)

$$\frac{\delta \operatorname{Re}_{j}}{\operatorname{Re}_{j}} = \left[ \left( \frac{\delta \nu}{\nu} \right)^{2} + \left( \frac{\delta Q_{j}}{Q_{j}} \right)^{2} + \left( \frac{\delta D_{j}}{D_{j}} \right)^{2} \right]^{1/2}$$
(3.14)

(5) Uncertainty of the nondimensional jet-disk separation distance  $HD_{j}$ ,

$$HD_{j} = \frac{H}{D_{j}}$$
(3.15)

$$\frac{\delta HD_{j}}{HD_{j}} = \left[ \left( \frac{\delta H}{H} \right)^{2} + \left( \frac{\delta D_{j}}{D_{j}} \right)^{2} \right]^{1/2}$$
(3.16)

The results from this uncertainty analysis are summarized in Table 3.1.

Parameter and Estimate Uncertainty	
Parameters	Uncertainty
$D_{j}, D_{w}, H(m)$	$\pm 0.00005 \text{ m}$
T (°C)	$\pm 0.2$ °C
$\Delta T$ (°C)	±0.3°C
Q <sub>j</sub> (slpm)	± 2%
μ (kg/ms)	$\pm 0.05\%$
$\rho$ (kg/m <sup>3</sup> )	$\pm 0.05\%$
$\upsilon$ (m <sup>2</sup> /s)	$\pm 0.07\%$
HD <sub>j</sub>	± 0.53%
Ra	± 8.4%
1896 III	
Rej	± 2.4%

## Table 3.1 Summary of uncertainty analysis
# **Chapter 4**

## **Results and Discussion**

It is noted that the flow characteristics associated with the confined air jet impinging onto the large heated disk under investigation are affected by the jet inertia, buoyancy force due to the heated disk, and the geometry of the injection pipe diameter and jet-disk separation distance. In the present experiment the injection pipe diameter is fixed at 20.0 mm and the jet-disk separation distance is chosen to be at 12.5 and 25.0 mm. The jet flow rate ranges from 0.4 to 10.0 slpm (standard liter per minute) and the temperature difference between the heated disk and the injected air is varied from 0 to 14.0°C. As noted in Chapter 3, the dimensionless groups governing the flow are the jet Reynolds number, Rayleigh number, and nondimensional jet-disk separation distance. They are respectively defined as

$$\operatorname{Re}_{j} = \frac{V_{j}D_{j}}{v} = \frac{4}{\pi} \frac{Q_{j}}{vD_{j}}$$
(4.1)

$$Ra = \frac{g\beta\Delta TH^3}{\alpha v}$$
(4.2)

$$HD_{j} = \frac{H}{D_{j}}$$
(4.3)

The Grashof number is defined as

$$Gr = \frac{g\beta\Delta TH^3}{v^2} = Ra / \Pr$$
(4.4)

Thus in the present study the jet Reynolds number  $\text{Re}_{j}$  ranges from 27 to 676, the Rayleigh number Ra from 0 to 7,340, the Grashof number Gr from 0 to 10,500 for  $\text{HD}_{j} = 0.625$  and 1.25. In what follows selected flow photos taken from side views and top views and the time records of the air temperature at selected locations are

examined closely to delineate how the gas flow and thermal characteristics are affected by the governing dimensionless groups. It should be mentioned that the vortex flow patterns in the confined impinging jet flow are found to be relatively different for H=25.0 mm and 12.5 mm. Hence the results for the two different jet-disk separation distances will be present separately.

#### 4.1 Vortex flow characteristics for H=25.0 mm

At first the vortex flow pattern observed for the limiting case of the unheated lower copper disk with  $\Delta T = 0^{\circ}C(Ra = 0)$  for the jet flow rate Q<sub>i</sub> varied from 1.5 to 6 slpm ( $Re_i = 101$  to 406) at long time when the flow already reaches steady state is illustrated in Fig. 4.1 for  $HD_i = 1.25$ . The results indicate that there exist two circular rolls in the test section. The mechanisms through which these two rolls are formed are examined closely. Specifically, upon impinging the heated plate the jet is deflected to move radially outward along the disk and slows down significantly due to the radial spread of the wall-jet flow. The wall-jet flow travels a certain distance from the hund stagnation point and then moves obliquely upwards as a result of the jet momentum is unable to overcome the wall friction and the retarding effects of the entrained flow by the upper confinement plate. Then, the oblique flow is divided into two streams as it encounters the upper plate. One stream moves radial inward toward the low pressure region created by the viscous shearing of the surrounding fluid associated with the jet injection, forming the inner roll which is therefore considered as the primary inertia-driven roll. Another stream moves outward along the upper plate for certain distance until it is unable to overcome the wall friction of upper plate. Then it descends gradually and flows outward. The phenomenon is often seen at low flow rate. But at a high flow rate, a smaller second roll is induced near the primary inertia-driven roll which is found to be driven by the viscous shearing effects

produced by the stronger and larger primary inertia-driven roll, which is termed as the secondary inertia-driven roll and has the opposite rotating direction with the primary inertia-driven roll. Besides, at decreasing flow rate both the primary and secondary inertia-driven rolls become weaker and smaller.

Next, the long time vortex flow patterns in the test section for the cases with the lower plate heated are shown in Figs. 4.2-4.5 for  $\Delta T = 2^{\circ}C \sim 5^{\circ}C$  and HD<sub>1</sub> = 1.25 at various jet flow rates by presenting the side flow photos at the statistical state. The results indicate that in addition to the primary and/or secondary inertia-driven rolls induced near the jet axis, several buoyancy-driven rolls appear in the outer region of the test section right above the edge of the heated plate even at the low temperature difference of 2°C (Fig. 4.2). More specifically, at the high Q<sub>i</sub> of 6 slpm two buoyancy rolls have been induced near the exit of the test section. These two rolls are respectively designated as the "first and second buoyancy rolls." As Q<sub>j</sub> is lowered to 5 slpm, the third buoyancy roll appears above the heated plate adjacent to the first and second buoyancy rolls. This process of new buoyancy roll generation continues at reducing jet flow rate. Note that at  $Q_i = 4$  and 3 slpm the fourth buoyancy roll appears and the fifth buoyancy emerges at  $Q_j = 2$  slpm. There are five buoyancy rolls in the test section for  $Q_j = 1.5$  slpm. Besides, the adjacent buoyancy rolls rotate in opposite directions. Similar vortex flow patterns at noted at higher  $\Delta T$ , as evident from the flow photos shown in Figs. 4.3-4.5.

It is important to note that the resulting vortex flows presented above do not reach steady state at long time even at the small  $\Delta T$  of 2°C. This can be attributed to the fact that the buoyancy rolls push each other and sometime merge of the buoyancy rolls occurs. The temporal evolution of the vortex flow pattern will be examined later. It is also noted that the vertical extent of the inertia-driven rolls reduces to a certain degree as the buoyancy-driven rolls appear. Besides, the buoyancy-driven rolls do not possess axisymmetry for all cases in Figs. 4.2-4.5. In fact, the vortex flow is somewhat irregular even at low buoyancy-to-inertia ratio. This is clearly seen from the long time top view flow photos shown in Figs. 4.6-4.9. The deformation of the buoyancy rolls is larger at a higher Ra or a lower Re<sub>j</sub>. Specifically, at a very low buoyancy-to-inertia ratio Gr/ Re<sub>j</sub><sup>2</sup> the vortex flow is dominated by the inertia-driven roll (Figs. 4.6(f), and 4.7(f) ). The buoyancy rolls are very weak. At slightly higher Gr/ Re<sub>j</sub><sup>2</sup> deformed buoyancy-driven circular rolls along with regular inertia-driven roll prevail such as that given in Figs. 4.6 (d) & (e), 4.7 (d) & (e). For a further increase in Gr/ Re<sub>j</sub><sup>2</sup> the buoyancy rolls become highly deformed especially these near the exit of the test section (Figs. 4.6 (c), and 4.7(c) ). For an even higher Gr/ Re<sub>j</sub><sup>2</sup> the buoyancy-driven vortex flow consists of irregular circular rolls, as is clear in Figs. 4.6(b) and 4.7(b). Some of these rolls in fact can be regarded as incomplete rolls. The inertia-driven roll also deforms to some degree. At a still higher Gr/ Re<sub>j</sub><sup>2</sup> the vortex rolls become highly irregular (Figs. 4.6(a), 4.7(a), 4.8(a) & (b), and 4.9(a) & (b)). Some of these rolls can be also regarded as incomplete rolls.

### 4.1.1 Effects of jet Reynolds number

The effects of the jet Reynolds number on the vortex flow patterns prevailed in the test section with H=25.0 mm can also be revealed from the results in Figs. 4.1-4.9. For a given  $\Delta T$  the strength and number of the buoyancy-driven rolls increases significantly at decreasing jet Reynolds number, obviously due to the increase in the buoyancy-to-inertia ratio. However, the inertia-driven rolls weaken at decreasing Re<sub>j</sub>, apparently owing to the reducing jet inertia. At the lowest Re<sub>j</sub> of 101 tested here the most inner buoyancy roll may contact with the primary inertia-driven roll for a high  $\Delta T$  (Figs. 4.4 & 4.5). Thus the interaction between the inertia- and buoyancy-driven vortex flows is stronger. Besides, at lower Re<sub>j</sub> the most outer buoyancy roll near the edge of the heated plate is much larger and stronger than the other buoyancy rolls.

#### 4.1.2 Effects of Rayleigh number

How the long time vortex flow pattern for H=25.0 mm is affected by the Rayleigh number is illustrated in Figs. 4.10-4.15 by showing the side view flow photos at increasing  $\Delta T$  for various Q<sub>j</sub> at the statistical state. The results indicate that an increase in the Rayleigh number for a given jet Reynolds number causes stronger and more buoyancy rolls to be induced in the test section. Besides, the sizes of the buoyancy rolls in the test section vary substantially even at the same Ra and Re<sub>j</sub>. The size of the most outer buoyancy-driven roll varies substantially for a change in Ra. It is of interest to note that in the presence of the buoyancy effect for  $\Delta T > 0^{\circ}C$  the primary inertia-driven roll becomes elongated in the radial direction when compared with that for  $\Delta T = 0^{\circ}C$ . This roll elongation is more prominent at a higher Ra.

### 4.1.3 Vortex flow evolution

Attention is then turned to examining the time evolution of the vortex flow induced in the test section at H=25.0 mm for selected cases at the statistical state. Figure 4.16 shows the side view flow photos at the selected time instants in the statistical state for the case with  $Re_j = 101$  and Ra = 2,940 ( $\Delta T = 2^{\circ}C$ ). The symbol "t = 0" denotes a certain time instant in the statistical state. Note that there are five buoyancy-driven rolls and one inertia-driven rolls in the test section. In the right half of the test section the variations of the roll size and strength with time are rather slight initially. But in the right half of the test section merge and split of the buoyancy rolls occur nonperiodically with time, causing significant changes in the roll size and pattern. In addition to the buoyancy roll, the downstream tip of the primary inertia-driven roll in the left half of the test section splits to form a new roll at t = 12s.

Later, the buoyancy rolls in the right half of the test section experience similar changes. The resulting vortex flow pattern is highly asymmetrical. Moreover, cyclic radial expansion and contraction of the buoyancy rolls are seen. At higher Ra for  $\Delta T = 3^{\circ}$ C the evolution of the vortex flow pattern is slightly quicker, as evident by comparing the results in Fig. 4.16 with Fig. 4.17. Besides, the radial extent of the primary inertia-driven roll varies noticeably with time. And the degree of the roll asymmetry is more severe. This trend continues for a further increase of  $\Delta T$  to 4°C and 5°C, as evident from the results shown in Figs. 4.18 and 4.19.

#### 4.1.4 Quantitative characteristics of buoyancy-driven rolls

In the impinging jet flow over a large heated disk investigated in the present study, the observed buoyancy-driven vortex flow presented above for H=25.0 mm is rather complicate. Here we summarize some important quantitative characteristics of the long time buoyancy-driven vortex flow in Table 4.1, which are deduced from the flow photos. These include the total number of the buoyancy rolls induced  $N_{BR}$  and the radial position of the center of the most inner buoyancy roll  $Z_{BR}$ . Besides,  $S_{BR2}$  denotes the maximum radial extent of the second buoyancy roll. Similar symbols are used for the other buoyancy rolls.

The data given in Table 4.1 are correlated empirically as follows. For the most inner buoyancy roll the radial location of the roll center can be correlated as  $Z_{BR}/H=$ 

$$-23.5+7.37*(Gr/Re_j^2)-63.1*(Gr/Re_j^2)^2+174*(Gr/Re_j^2)^3-188*(Gr/Re_j^2)^4$$
  
+69.2\*(Gr/Re\_j^2)^5+275/(N\_{BR})-932/(N\_{BR})^21330/(N\_{BR})^3-648/(N\_{BR})^4  
for  $101 \le Re_j \ge 406$  and  $1470 \le Ra \ge 7,340$  (4.5)

The maximum radial extents of the second to fifth buoyancy-driven rolls counting from the most outer buoyancy roll can be correlated respectively as

$$\begin{split} &S_{BR2}/H = (Gr/Re_j^2) \quad (Z_{BR}/H) \\ &20.4-48.4^*(Gr/Re_j^2) - 17.5^*ln(Z_{BR}/H) + 56.1^*(Gr/Re_j^2)^2 + 3.8^*(ln(Z_{BR}/H))^2 \\ &+ 23.9^*(Gr/Re_j^2)^*ln(Z_{BR}/H) - 13.52^*(Gr/Re_j^2)^3 + 0.0056^*(LN(Z_{BR}/H))^3 \\ &+ 0.032^*(LN(Z_{BR}/H))^{2*} (Gr/Re_j^2) - 21.53^*(Gr/Re_j^2)^{2*}ln(Z_{BR}/H) \\ &\text{for } 101 \leq Re_j \geq 406 \text{ and } 1470 \leq Ra \geq 7,340, \end{split}$$

 $S_{BR3}/H$ 

$$= 574-2.77(Gr/Re_{j}^{2})+15.8*(Gr/Re_{j}^{2})^{2}-55.4*(Gr/Re_{j}^{2})^{3}$$

$$+77.7*(Gr/Re_{j}^{2})^{4}-35.4*(Gr/Re_{j}^{2})^{5}-605*(Z_{BR}/H)^{2}$$

$$+250*(Z_{BR}/H)^{2}-51*(Z_{BR}/H)^{3}+5.1*(Gr/Re_{j}^{2})^{4}-0.2*(Gr/Re_{j}^{2})^{5}$$
for  $101 \le Re_{j} \ge 406$  and  $1470 \le Ra \ge 7,340$ , (4.7)

 $S_{BR4}/H$ 

$$= -0.84 - 0.165 * \ln(Gr/Re_{j}^{2}) - 0.04 * (\ln(Gr/Re_{j}^{2}))^{2.5} + 0.028 * (\ln(Gr/Re_{j}^{2}))^{3} + 0.0045 * (Gr/Re_{j}^{2})^{4.5} + 3.26 * (Z_{BR}/H) - 1.65 * (Z_{BR}/H)^{2.5} + 0.52 * (Z_{BR}/H)^{3} - 0.076 * (Z_{BR}/H)^{4.5} + 0.085 * (Z_{BR}/H)^{5}$$
for  $101 \le Re_{j} \ge 406$  and  $1470 \le Ra \ge 7,340$ , (4.8)

and

 $S_{BR5}/H$ 

$$= 568-0.163*(Gr/Re_{j}^{2})+5.50*(Gr/Re_{j}^{2})^{2.5}-4.89*(Gr/Re_{j}^{2})^{3}-151*(Z_{BR}/H)$$
  
+276\*(Z<sub>BR</sub>/H)<sup>0.5</sup>\*ln(Z<sub>BR</sub>/H)-0.618\*(ln(Z<sub>BR</sub>/H))<sup>2</sup>-426\*ln(Z<sub>BR</sub>/H)  
-185/ln(Z<sub>BR</sub>/H)  
for 101≤ Re\_{j} ≥ 406 and 1470≤ Ra ≥ 7,340 (4.9)

When compared with the present measured data, the standard deviations of the above five correlations are 3.4%, 8.4%, 13.2%, 15.5%, and 1.2%, individually.

### 4.1.5 Thermal characteristics

The time records of the non-dimensional air temperature, defined as  $(T-T_j)$  /

 $(T_f-T_j)$  at selected locations are presented in Figs.4.20-4.27 for various Re<sub>j</sub> and Ra at H=25.0 mm. The results indicate that for the air jet impinging onto the large heated plate the air temperature is in unstable oscillation since the resulting vortex flow is unable even at low buoyancy-to-inertia ratio. In fact, nonperidic flow oscillation prevails for all cases with a high frequency oscillation component superimposed on a low frequency oscillation.

#### 4.1.6 Flow regime map

Based on the results obtained in the present study, a flow regime map in terms of Ra vs. Re<sub>j</sub> for the cases with H = 25 mm is given in Fig. 4.28 to delineate the parameter domains for the identified three different buoyancy-driven vortex flow patterns induced in the confined impinging jet. These include the nearly regular circular roll pattern, incomplete vortex roll pattern, and irregular roll pattern. The results in this plot manifest that at low buoyancy-to-inertia ratio  $Gr/Re_j^2$  the nearly regular vortex flow prevails and at high  $Gr/Re_j^2$  the irregular vortex flow eliminates. Besides, the incomplete circular rolls predominate at the intermediate  $Gr/Re_j^2$ . The boundaries separating the different vortex flow patterns are correlated empirically.

First, the boundary separating the irregular and incomplete vortex rolls can be correlated as

$$Ra = 885 + 0.089* Re_{i}^{2}$$
(4.10)

for 101<Rei<406 and 1470<Ra<7,340

and the standard deviations is 9.5%.

Then, the boundary between the incomplete and regular vortex rolls can be correlated as

$$Ra = 4010 + 0.551 * Re_{i}^{1.5}$$
(4.11)

for 101<Rei<406, and 1470<Ra<7,340

and the standard deviations is 1.6%.

#### 4.2 New vortex flow patterns at H=12.5 mm

It is of interest to note in the flow visualization that two new vortex flow patterns appear when the jet-disk separation distance is reduced to 12.5 mm. More specifically, we observed radial rolls and moving circular waves in certain ranges of the jet Reynolds number and Rayleigh number. The top view flow photos taken at the midheight of the test section are presented in Figs. 4.29-4.42 for various Rei and Ra to illustrate these new vortex flow patterns. The results given in Fig. 4.29 for Ra=1,470  $(\Delta T=8^{\circ}C)$  at Re<sub>i</sub> increased from 101 to 676 show that a few moving circular waves appear in the outer zone of the test section at the small Re<sub>i</sub> of 101. These waves are slightly deformed and do not possess axisymmetry. Besides, they move in the radial direction and their wave fronts are normal to the direction of the wall jet flow. Hence they are essentially the transverse waves. For an increase of Rei to 135 several radial rolls are induced, in addition to the weaker moving waves (Fig. 4.29(b)). Note that the radial rolls originate in the stagnation region of the impinging jet near the jet axis and grow in size in the radial direction. But the size of the induced radial rolls in the test section for the given Rei and Ra varies noticeably in the circumferential direction. Some radial rolls are large than the other. As the jet Reynolds number is raised to 203 and high level, no moving waves and radial rolls are seen. Instead, the flow in the test section is dominated by the primary and secondary inertia-driven circular rolls (Figs. 4.29(c)-(j)).

To ascertain the conditions leading to the appearance of the new vortex flow structures, we repeat the above experiment for a smaller interval of the jet Reynolds number. The obtained top view flow photos are shown in Fig. 4.30 for  $Re_j$  ranging from 27 to 149. The results indicate that the deformed moving waves prevail for  $Re_j$  as low as 27. As  $Re_j$  is raised to 88 both the moving waves and radial rolls appear in

the test section (Fig. 4.30(j)).

Next, the results presented in Figs. 4.31-4.34 for slightly higher  $\Delta T$  of 9°C and 10°C show that the moving waves and radial rolls appear in nearly the same range as that for  $\Delta T=8^{\circ}C$ . For a further raise of  $\Delta T$  to 11°C the moving waves exist in a slightly smaller range of Re<sub>i</sub> (27 to 68). But the pattern characterized by the simultaneous presence of the radial rolls and moving waves, which is designated as "the mixed roll-wave pattern", prevails in a slightly wider range of Re<sub>i</sub> (101 to 135), as evident from Fig. 4.36. At the even higher  $\Delta T$  of 12°C the range of Re<sub>i</sub> for the appearance of the moving waves is even smaller (27 to 61) and the mixed roll-wave pattern dominates in a wider Re<sub>i</sub> range (68 to 115). Note that for Re<sub>i</sub> ranging from 122 to 149 only the radial rolls appear and no moving waves are seen (Figs. 4.37 and 4.38). For Re<sub>i</sub> larger than 149 the flow is dominated by the primary inertia-driven and buoyancy-driven rolls. For a still higher  $\Delta T$  of 13°C the results in Figs. 4.39 and 4.40 indicate that the moving waves dominate for Rei ranging from 27 to 54 and the mixed pattern appears in a wider Rei range of 61 to 108. Besides, the radial rolls are prevalent for a wider range of Re<sub>i</sub> (115 to 149). As  $\Delta T$  is raised to 14 °C Figs. 4.41 and 4.42 show that buoyancy roll prevails at low Rei and the moving waves only appear at  $Re_i = 27$  to 41. For  $47 \le Re_i \le 88$  the mixed pattern dominates. And the radial rolls fill the test section for  $95 \leq \text{Re}_{i} \leq 149$ .

Selected data for the measured time records of the non-dimensional air temperature are presented in Figs. 4.43-4.49 for various  $Re_j$  and Ra at H=12.5 mm. The results indicate that the air temperature also oscillates irregularly with time when the new vortex flow patterns dominate in the test section.

The result presented above clearly indicate that three new vortex flow patterns have been identified in the present study. These patterns include the vortex flow dominates by the pure moving circular waves, the pure radial rolls, and the coexistence of the moving waves and radial rolls. The range of  $Re_j$  and Ra for the appearance of these new vortex flow patterns are presented in flow regime maps given in Figs. 4.50 and 4.51 for H=12.5 mm.

The boundary separating the transversal waves and mixed roll-wave pattern can be correlated as

$$Ra = 3470 - 2.55 * Re_{i}^{1.5}$$
(4.12)

for 20<Rej<676 and 1,470<Ra<2,670

and the standard deviations is 8.4%.

Besides, the boundary between the mixed roll-wave pattern and radial rolls can be correlated as

$$Ra= 3770-1.14*Re_{j}^{1.5}$$
(4.13)  
for 20and the standard deviations is 2.3%. Then, the boundary separating the radial roll pattern and the pattern consisting of the  
primary inertia-driven roll and buoyancy-driven rolls can be correlated as  
$$Ra=4502-1.05*Re_{j}^{1.5}$$
(4.14)

for 20<Rej<676 and 1,470<Ra<2,670

and the standard deviations is 2.5%.

Finally, the boundary separating the pattern including the primary inertia-driven roll and buoyancy-driven rolls and the pattern consisting of the primary inertia-driven roll, secondary inertia-driven roll, and buoyancy-driven rolls can be correlated as

$$Ra = -125 + 0.291 * Re_{j}^{1.5}$$
(4.15)

for 20<Rej<676 and 1,470<Ra<2,670

and the standard deviations is 14.1%.

ΔΤ	Q <sub>j</sub> (slpm)	Rej	Gr/Re <sub>j</sub> <sup>2</sup>	N <sub>BR</sub>	Z <sub>BR</sub> /H	S <sub>BR2</sub> /H	$S_{BR3}/H$	S <sub>BR4</sub> /H	S <sub>BR5</sub> /H
2°C	1.5	101	0.408	5	3.12	1.2	1.04	0.96	0.90
	2	135	0.229	5	4.24	1.04	1	0.96	0.88
	3	203	0.102	4	5.68	1.2	0.8	0.72	Х
	4	270	0.057	4	6	1.0	0.96	0.64	Х
	5	338	0.037	3	6.32	1.2	0.96	Х	Х
	6	406	0.025	2 🕇	7.36	0.72	Х	Х	Х
3°C	1.5	101	0.611	5	4.72	0.96	0.88	0.8	0.76
	2	135	0.344	4	5.28	0.96	0.88	0.76	Х
	3	203	0.153	4	5.52	0.96	0.88	0.66	Х
	4	270	0.086	2	6.72	0.8	Х	Х	Х
	5	338	0.055	2	6.88	0.76	Х	Х	Х
	6	406	0.038	1	X	X	Х	Х	Х
4°C	1.5	101	0.815	5	4.24	1.2	1.08	0.72	0.64
	2	135	0.459	( 4 E	4.88	0.88	0.8	0.72	Х
	3	203	0.204	3	6.16	0.88	0.8	Х	Х
	4	270	0.115	2	6.96	0.8	Х	Х	Х
	5	338	0.073	2	6.88	0.96	Х	Х	Х
	6	406	0.051	1	X	X	Х	Х	Х
5°C	1.5	101	1.019	5	4	0.96	0.88	0.8	0.72
	2	135	0.573	5	4.32	0.8	0.72	0.64	0.56
	3	203	0.255	4	5.76	0.72	0.64	0.6	Х
	4	270	0.143	3	5.92	0.96	0.88	X	X
	5	338	0.092	3	5.84	0.96	0.88	Х	X
	6	406	0.064	3 🕇	6.16	0.96	0.88	X	X

Table 4.1 The characteristics of buoyancy-driven rolls



Fig.4.1 Steady side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° for various jet Reynolds numbers at Ra=0 ( $\Delta T=0^{\circ}C$ ) for H=25.0mm.



Fig.4.1 continued



Fig.4.2 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various jet Reynolds numbers at Ra=2940 ( $\Delta T=2^{\circ}C$ ) for H=25.0mm.



Fig.4.3 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various jet Reynolds numbers at Ra=4400 ( $\Delta T=3^{\circ}C$ ) for H=25.0mm.



Fig.4.4 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various jet Reynolds numbers at Ra=5870 ( $\Delta$ T=4°C) for H=25.0mm.



Fig.4.5 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various jet Reynolds numbers at Ra=7340 ( $\Delta T=5^{\circ}C$ ) for H=25.0mm.





(c)

(d)



Fig.4.6 Top view flow photos taken at midheight of the test section with Ra=2,940 ( $\Delta T=2^{\circ}C$ ) & H=25.0 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.7 Top view flow photos taken at midheight of the test section with Ra=4,400 ( $\Delta T=3^{\circ}C$ ) & H=25.0 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.8 Top view flow photos taken at midheight of the test section with Ra=5,870 ( $\Delta$ T=4°C) & H=25.0mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.9 Top view flow photos taken at midheight of the test section with Ra=7,340 ( $\Delta T=5^{\circ}C$ ) & H=25.0 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Jet

Fig.4.10 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 1.5$  (Re<sub>j</sub>=101) slpm for H=25.0mm



Fig.4.11 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 2$  slpm (Re<sub>j</sub>=135) for H=25.0mm



Fig.4.12 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 3$  slpm (Re<sub>j</sub>=203) for H=25.0mm



Fig.4.13 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 4$  slpm (Re<sub>j</sub>=270) for H=25.0mm



Fig.4.14 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 5$  slpm (Re<sub>j</sub>=338) for H=25.0mm



Fig.4.15 Side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180° at statistical state for various  $\Delta T$  at  $Q_j = 6$  slpm (Re<sub>j</sub>=406) for H=25.0mm



Fig.4.16 Vortex flow evolution for H=25.0mm at Re<sub>j</sub>=101 (Q<sub>j</sub>=1.5 slpm) and Ra=2,940 ( $\triangle T=2^{\circ}C$ ) illustrated by side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180°.



Fig.4.16 Continued







Fig.4.16 Continued



Fig.4.17 Vortex flow evolution for H=25.0mm at Re<sub>j</sub>=101 (Q<sub>j</sub>=1.5 slpm) and Ra=4,400 ( $\triangle T=3^{\circ}C$ ) illustrated by side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180°.



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Fig.4.17 Continued



Fig.4.17 Continued



Fig.4.17 Continued


Fig.4.17 Continued



Fig.4.17 Continued



Fig.4.18 Vortex flow evolution for H=25.0mm at Re<sub>j</sub>=101 (Q<sub>j</sub>=1.5 slpm) and Ra=5,870 ( $\triangle$ T=4°C) illustrated by side view flow photos taken at the cross plane  $\theta$ =0° & 180°.



59

Fig.4.18 Continued



Jet

60

Fig.4.18 Continued



Jet

Fig.4.18 Continued



Fig.4.18 Continued



Fig.4.18 Continued



Fig.4.18 Continued



Fig.4.18 Continued



Fig.4.18 Continued



Fig.4.19Vortex flow evolution for H=25.0mm at Re<sub>j</sub>=101 (Q<sub>j</sub>=1.5 slpm) and Ra=7,340 ( $\triangle T=5^{\circ}C$ ) illustrated by side view flow photos taken at the cross plane  $\theta=0^{\circ}$  & 180°.



Fig.4.19 Continued



Fig.4.19 Continued



Fig..4.20 The time records of non-dimensional air temperature for Ra=2,940 ( $\Delta T=2$  °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.95 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.21 The time records of non-dimensional air temperature for Ra=4,400 ( $\Delta T$ =3 °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.95 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.22 The time records of non-dimensional air temperature for Ra=5,870 ( $\Delta$ T=4 °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.95 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.23 The time records of non-dimensional air temperature for Ra=7,340 ( $\Delta T$ =5 °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.95 for various Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig..4.24 The time records of non-dimensional air temperature for Ra=2,940 ( $\Delta T=2$  °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.75 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.25 The time records of non-dimensional air temperature for Ra=4,400 ( $\Delta T$ =3 °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.75 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.26 The time records of non-dimensional air temperature for Ra=5,870 ( $\Delta$ T=4 °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.75 for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.27 The time records of non-dimensional air temperature for Ra=7,340 ( $\Delta T=5$  °C) & H=25.0 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.75 for various Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, and (f)406.



Fig.4.28 Flow regime map delineating irregular and regular buoyancy-driven rolls for H = 25.0 mm.



(a)



Fig. 4.29 Top view flow photos taken at midheight of the test section with Ra=1,470( $\Delta T=8^{\circ}C$ ) & D<sub>j</sub>=20.0 mm at H=12.5 mm for  $Re_j$ = (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f)406, (g) 473, (h)541, (i) 609, and (j)676



(f)



(g)





(j)

Fig. 4.29 continued.



Fig.4.30 Top view flow photos taken at midheight of the test section with Ra=1,470 ( $\Delta T=8^{\circ}C$ ) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)27, (b) 34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122, (p) 128, (q) 135, (r) 142, and (s) 149.







(j)

Fig.4.30 continued.



(1)





(0)

Fig.4.30 continued.







Fig.4.30 continued.





Fig.4.31 Top view flow photos taken at midheight of the test section with Ra=1,650( $\Delta T=9^{\circ}C$ ) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f)406, (g) 473, (h)541, (i) 609, and (j) 676.









(j)

Fig.4.31 continued



ALL R (c) (d)



Fig.4.32 Top view flow photos taken at midheight of the test section with Ra=1,650 ( $\Delta T=9^{\circ}C$ ) & D<sub>j</sub>=20.0 mm at H=12.5 mm for  $\text{Re}_j$ = (a) 27, (b)34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122, (p) 128, and (q) 135.



(g)







(k)

Fig.4.32 continued.



(1)





(q)

Fig.4.32 continued.



(a)





Fig.4.33 Top view flow photos taken at midheight of the test section with Ra=1,840( $\Delta T$ =10°C) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f) 406, (g) 473, (h) 541, (i) 609,and (j) 676.



(f)



(h)



(j)

Fig. 4.33 Continued.


Fig.4.34 Top view flow photos taken at midheight of the test section with Ra=1,840 ( $\Delta T$ =10°C) &  $D_j=20.0 \text{ mm}$  at H=12.5 mm for  $Re_j=(a)27, (b)34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 88, (h) 74, (h) 81, (h) 81$ (k) 95, (l) 101, (m) 108, (n) 115, (o) 122, (p) 128, (q) 135, and (r)142 .  $_{92}^{92}$ 



(g)









(1)

Fig.4.34 continued.



(m)



ALL RADIES 5910 (0) (p)





(q)

(r)

Fig.4.34 continued.



(a)





Fig.4.35 Top view flow photos taken at midheight of the test section with Ra=2,020( $\Delta T$ =11°C) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f) 406, (g) 473, (h) 541, (i) 609,and (j) 676.









(j)

Fig. 4.35Continued.





(c)



Fig.4.36 Top view flow photos taken at midheight of the test section with Ra=2,020 ( $\Delta T$ =11°C) &  $D_j=20.0 \text{ mm}$  at H=12.5 mm for  $Re_j=(a)27$ , (b) 34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122, (p) 128,(q) 135, (r) 142, and (s) 149.



(f)







(j)

Fig.4.36 continued.







(0)

Fig.4.36 continued.







Fig.4.36 continued.



(a)





Fig.4.37Top view flow photos taken at midheight of the test section with Ra=2,200( $\Delta T$ =12°C) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f) 406, (g) 473, (h) 541, (i) 609,and (j) 676.



(h)



(j)

Fig. 4.37continued.





Fig.4.38 Top view flow photos taken at midheight of the test section with Ra=2,200 ( $\Delta T=12^{\circ}C$ ) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)27, (b) 34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122, (p) 128,(q) 135, (r) 142,and (s) 149.



(h)



(j)

Fig.4.38 continued.







(0)

Fig.4.38 continued.







Fig.4.38continued.







Fig.4.39 Top view flow photos taken at midheight of the test section with Ra=2,390( $\Delta T$ =13°C) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f) 406, (g) 473, (h) 541, (i) 609,and (j) 676.









(j)

Fig.4.39 continued.





(f)

Fig.4.40 Top view flow photos taken at midheight of the test section with Ra=2,390 ( $\Delta T=13^{\circ}C$ ) &  $D_j=20.0 \text{ mm}$  at H=12.5 mm for  $Re_j=$  (a) 27, (b) 34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 61, (g) 68, (h) 74, (i) 81, (g) 68, (h) 74, (i) 81, (g) 68, (h) 74, (h) 81, (g) 81, (g 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122,(p) 128, (q) 135,and (r) 142.



(g)







(k)



(1)

Fig.4.40 continued.



(m)







(q)



(r)





Fig.4.41 Top view flow photos taken at midheight of the test section with Ra=2,570( $\Delta T$ =14°C) & D<sub>j</sub>=20.0 mm at H=12.5 mm for Re<sub>j</sub>= (a)101, (b) 135, (c) 203, (d) 270, (e) 338, (f) 406, (g) 473, (h) 541, (i) 609,and (j) 676.







(j)

Fig. 4.41 Continued.



(f)

Fig.4.42 Top view flow photos taken at midheight of the test section with Ra=2,670 ( $\Delta T=14^{\circ}C$ ) &  $D_j=20.0 \text{ mm}$  at H=12.5 mm for  $Re_j=$  (a) 27, (b) 34, (c) 41, (d) 47, (e) 54, (f) 61, (g) 68, (h) 74, (i) 81, (j) 61, (g) 68, (h) 74, (i) 81, (j) 61, (g) 68, (h) 74, (i) 81, (g) 68, (h) 74, (i) 81, (g) 68, (h) 74, (h) 81, (g) 81, (h) 81, (h 88, (k) 95, (l) 101, (m) 108, (n) 115, (o) 122,(p) 128, (q) 135,and (r) 142.



(g)







(k)

(1)

Fig.4.42 continued.



(m)







(q)



(r)

Fig.4.42 continued.



Fig.4.43 The time records of non-dimensional air temperature for Ra=1,470 ( $\Delta T=8^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.44 The time records of non-dimensional air temperature for Ra=1,650 ( $\Delta T=9^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.45 The time records of non-dimensional air temperature for Ra=1,840 ( $\Delta T=10^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135,and (h) 149.



Fig.4.46 The time records of non-dimensional air temperature for Ra=2,020 ( $\Delta T=11^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.47 The time records of non-dimensional air temperature for Ra=2,200 ( $\Delta T=12^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.48 The time records of non-dimensional air temperature for Ra=2,390 ( $\Delta T=13^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.49 The time records of non-dimensional air temperature for Ra=2,570 ( $\Delta T=14^{\circ}C$ ) & H=12.5 mm measured at selected locations on the vertical plane  $\theta = 0^{\circ}$  at Z = 0.5 and R = r/R<sub>c</sub> = 0.9 for Re<sub>j</sub>= (a) 34, (b) 47, (c) 68, (d) 81, (e) 101, (f) 115, (g) 135, (h) 149.



Fig.4.50 Flow regime map delineating primary inertia-driven roll, buoyancy-driven rolls, transversal waves, and radial rolls for H = 12.5 mm.





## **CHAPTER 5**

## **CONCULDING REMARKS**

An experiment combining flow visualization and temperature measurement is conducted in the present study to explore the inertia- and buoyancy-driven vortex flow resulting from a round air jet impinging onto a large confined heated horizontal circular disk. Particular attention is paid to examining the effects of Re<sub>j</sub> and Ra on the appearance of new vortex flow patterns. In this experiment the jet-disk separation distance is varied from 12.5 and 25.0 mm, the jet Reynolds number from 20 to 676, and the Rayleigh number from 0 to 7,340. The major results obtained in the present study can be briefly summarized in the following:

1. The results from the flow visualization for H=25.0 mm indicate that the vortex flow is characterized by the primary and/or secondary inertia-driven circular rolls along with several buoyancy-driven rolls. The number of the buoyancy induced rolls increases with the buoyancy-to-inertia ratio, which can vary from 1 to 5. Besides, at a low Gr/Rej<sup>2</sup> slightly deformed circular buoyancy rolls prevail in the test section. For slightly higher Gr/Rej<sup>2</sup> the flow is dominated by the highly deformed curved rolls. The roll pattern becomes somewhat irregular for a further increase in Gr/Rej<sup>2</sup>. For all cases examined here the vortex flow is unsteady at long time after the initial transients have died out and is irregular to a certain degree since the buoyancy effect is rather strong for the large impinging plate tested here. In addition to the roll deformation, the mutual pushing, merging and splitting of the buoyancy rolls occur nonperiodically in time. This unsteady and irregular vortex flow is also reflected in the data for the air

temperature variations with time. Some quantitative buoyancy-driven vortex flow characteristics such as the size and location of the buoyancy rolls are summarized and correlated empirically. Moreover, a flow regime map is provided to delineate various induced vortex flow patterns and the boundaries separating various vortex flow patterns are also correlated empirically.

2. When the jet-disk separation distance is reduced to 12.5 mm, circular waves traveling in the radial direction and radial vortex rolls appear in the confined impinging jet flow. These waves are somewhat deformed and are not axisymmetric. The radial rolls originate in the stagnation region of the impinging jet and grow in size in the radial direction. The size of the radial rolls is also nonuniform in the circumferential direction. Besides, the moving waves and radial rolls can coexist in the flow. Moreover, the ranges of the jet Reynolds number and Rayleigh numbers leading to the new vortex flow patterns are determined.
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